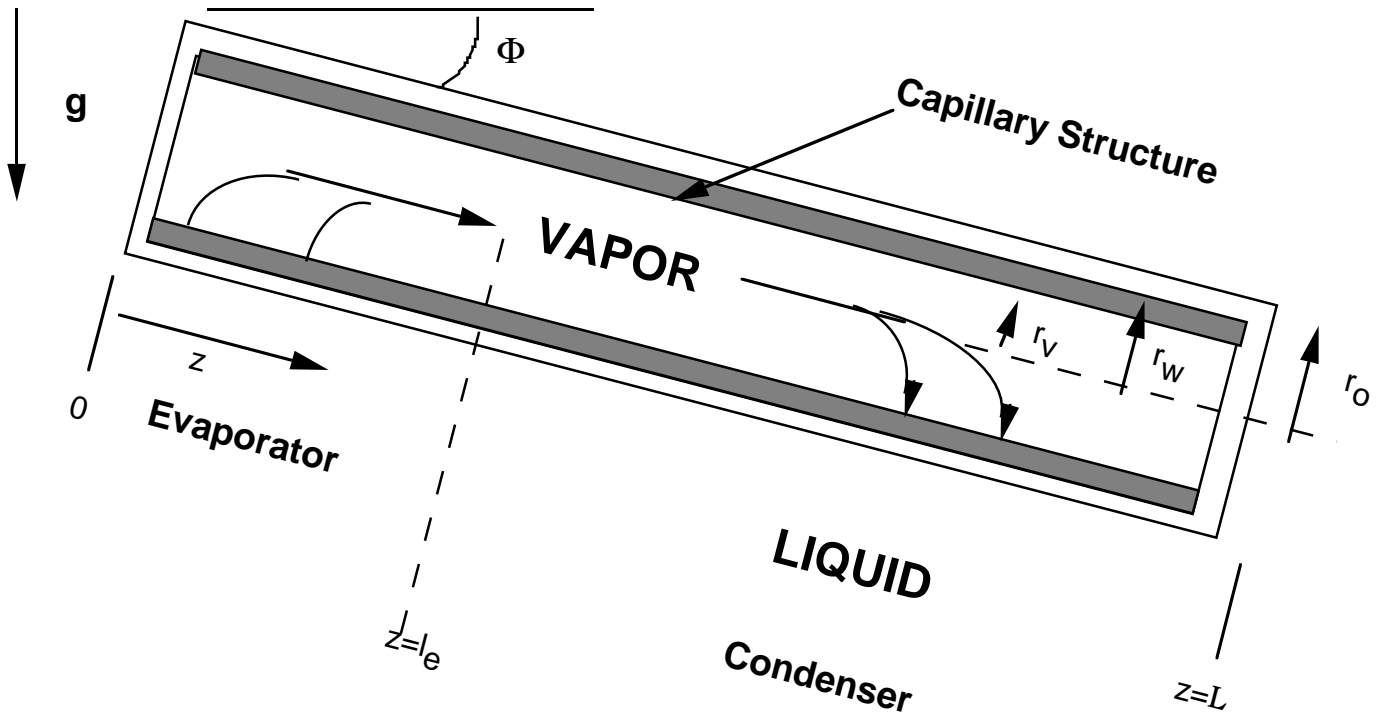


# Heat Pipe Principles

Use 2 phase flow, latent heat of vaporization, and capillary action to circulate a working fluid between heated and cooled regions via a wick.

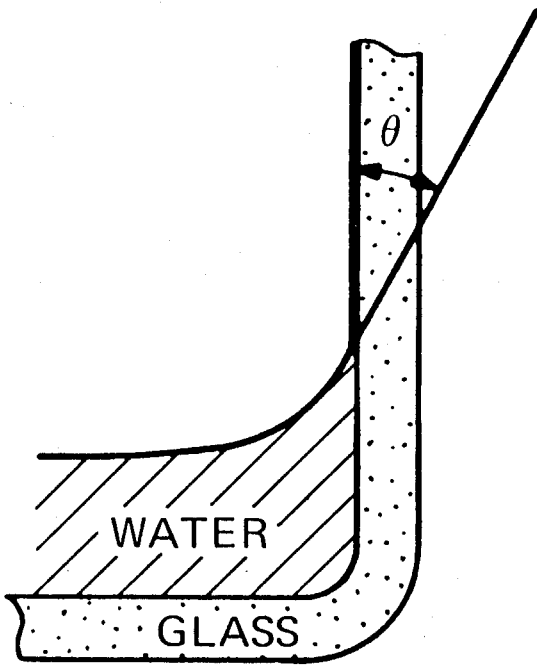


$r_o$  = outer radius

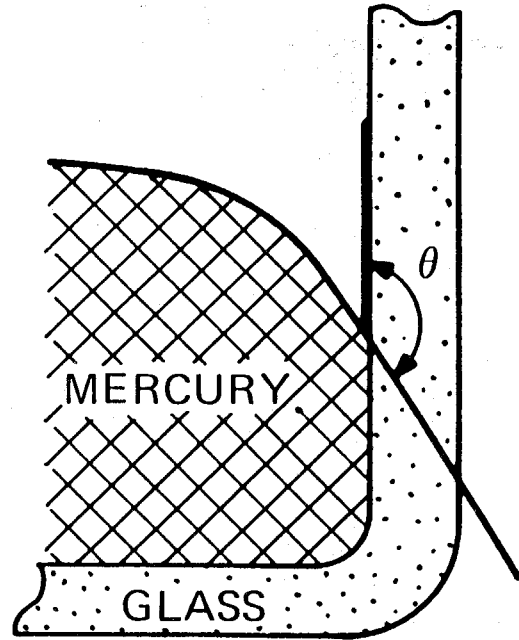
$r_w$  = inner radius of wick

$r_v$  = radius of free space in tube

$l_e$  = length of evaporation regime



WETTING



NON-WETTING

{ NOTE:  $\theta = \text{CONTACT } \angle$

DIMENSIONS EXAGGERATED

**Fig. 4.9** Wetting of a solid surface. *Courtesy of Los Alamos National Laboratory.*

## Capacity of Heat Pipe

- Increase in heat transfer must be consistent with capillary driven circulation of the working fluid.

**Difference in pressure between the vapor phase,  $p_v(z)$ , and the liquid phase  $p_l(z)$ , must be balanced by the surface tension in the capillary structure.**

$$p_v(z) - p_l(z) = \Delta p_v - \Delta p_l = \frac{2\gamma \cos \theta}{r_c}$$

**radius of capillary pore**

$$\Delta p_l = -p_l(L) + p_l(0)$$

$$\Delta p_l = -\rho_l g L \sin \varphi - \frac{\text{Constant } b \eta_l Q_e L}{2\pi(r_w^2 - r_v^2)\rho_l \epsilon r_c^2 l}$$

**Density of Liquid** (points to  $\rho_l$ )

**Acceleration due to gravity** (points to  $g$ )

**Angle to gravity**  
 $\Phi = \pi/2$  vertical  
 $\Phi = 0$  horizontal (points to  $\sin \varphi$ )

**Frac. of Wick Vol. Occ. by Liquid** (points to  $\epsilon$ )

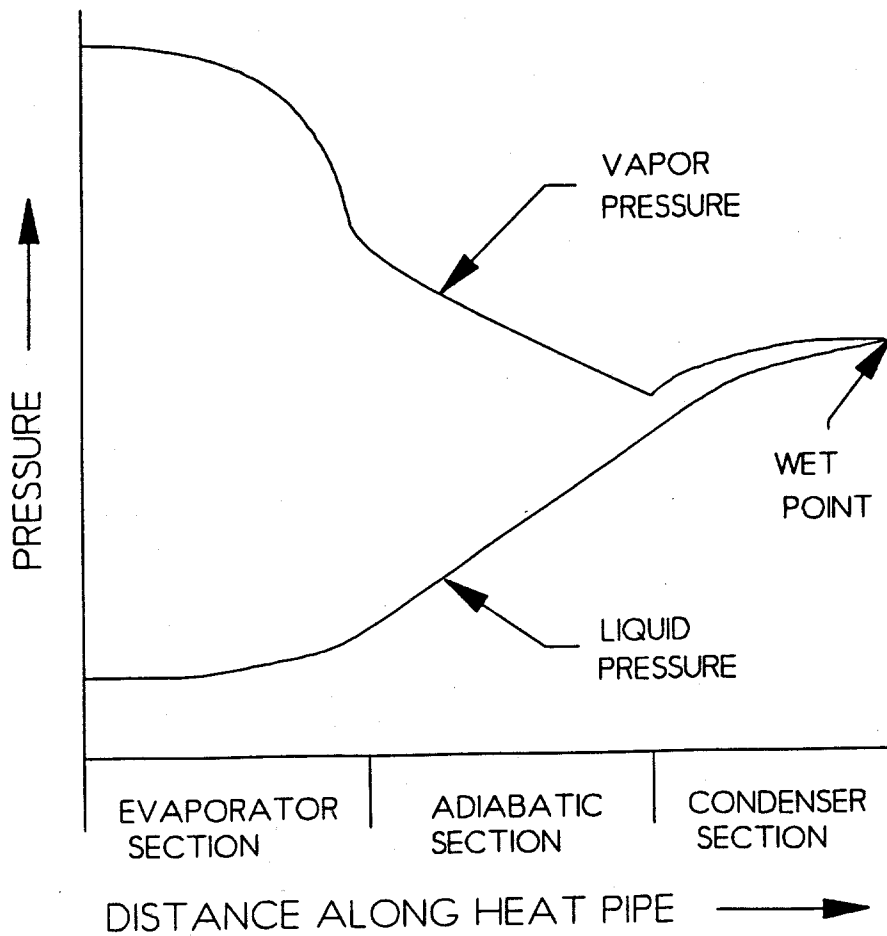
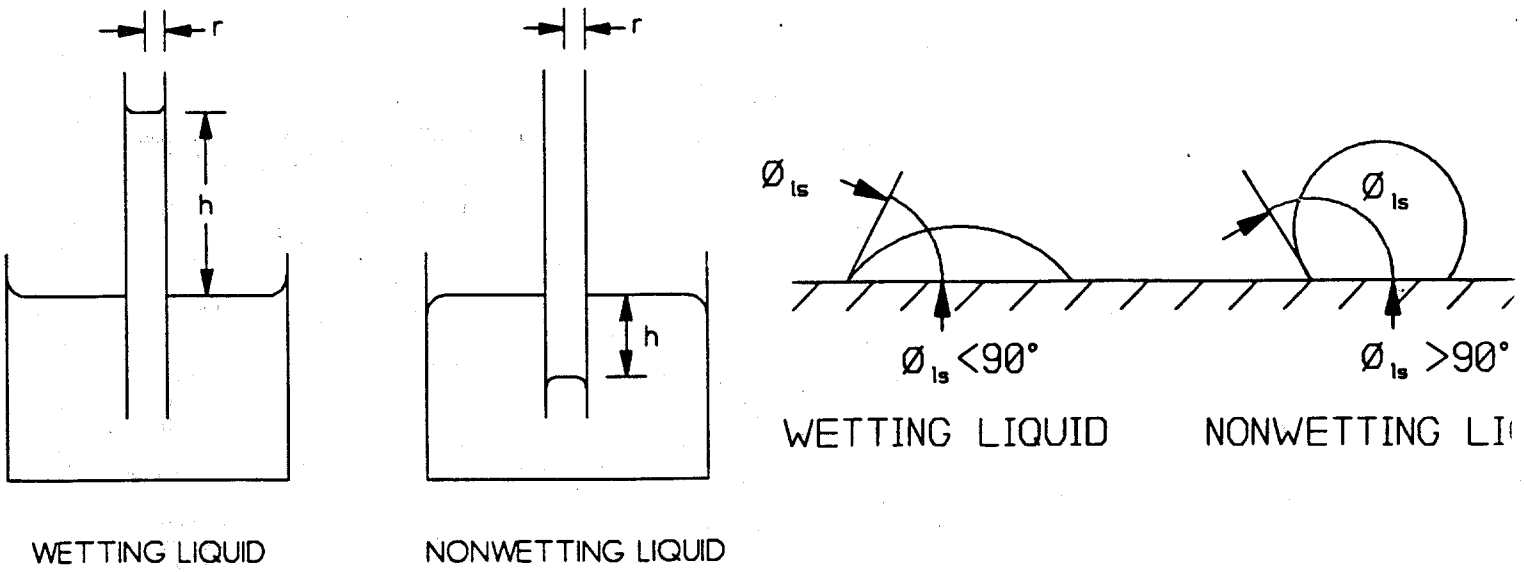


Figure 2.5. Liquid and vapor pressure distributions in a heat pipe (wet point at condenser end).

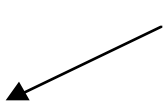
## Value of Constant 'b'

If pores are not interconnected, then  $b \approx 8$

If the pores are interconnected, then  $b \approx 10-20$

**Optimum Pore Size** (see Ref 10 Book by Silverstein)

**Viscosity of liquid**


$$r_c = \frac{b\eta_l Q_e L}{4\pi(r_w^2 - r_v^2)\rho_l \varepsilon l \gamma \cos \theta}$$

## Maximum Heat Transport

$$Q_e = \frac{\pi r_w^2 l \gamma \cos \theta}{3L} \sqrt{\frac{\varepsilon \rho_v \rho_l}{3b\eta_v \eta_l}}$$

**(Reynolds # << 1)**

$$Q_e = \frac{4\pi r_w^2 l}{3} \left[ \frac{2\rho_v \rho_l \varepsilon \gamma^2 \cos^2 \theta}{(\pi^2 - 4)bL\eta} \right]^{\frac{1}{3}}$$

**(Reynolds # >> 1)**

# Surface\_Tension.xls

<i>Surface Tension of Some Heat Pipe Liquids</i>		
	T-°C	Gamma-N/cm
Methyl Alcohol	50	2.01
Ammonia	11	2.35
Water	20	7.28
Na	816	12.1
Li	1204	26

## **Key Features of High Temperature Heat Pipes**

- **Extremely high heat transfer in a simple container**
- **Allows many heat transfer loops, avoiding a single point failure**
- **Smaller units avoid bulky pressure vessel (implications for reentry)**
- **Avoids the use of valves, pumps or compressors**
- **Ability to start up 'cold' avoids the need for preheat**
- **Nearly isothermal temperature transfer and high temperatures allows very high efficiency operation**

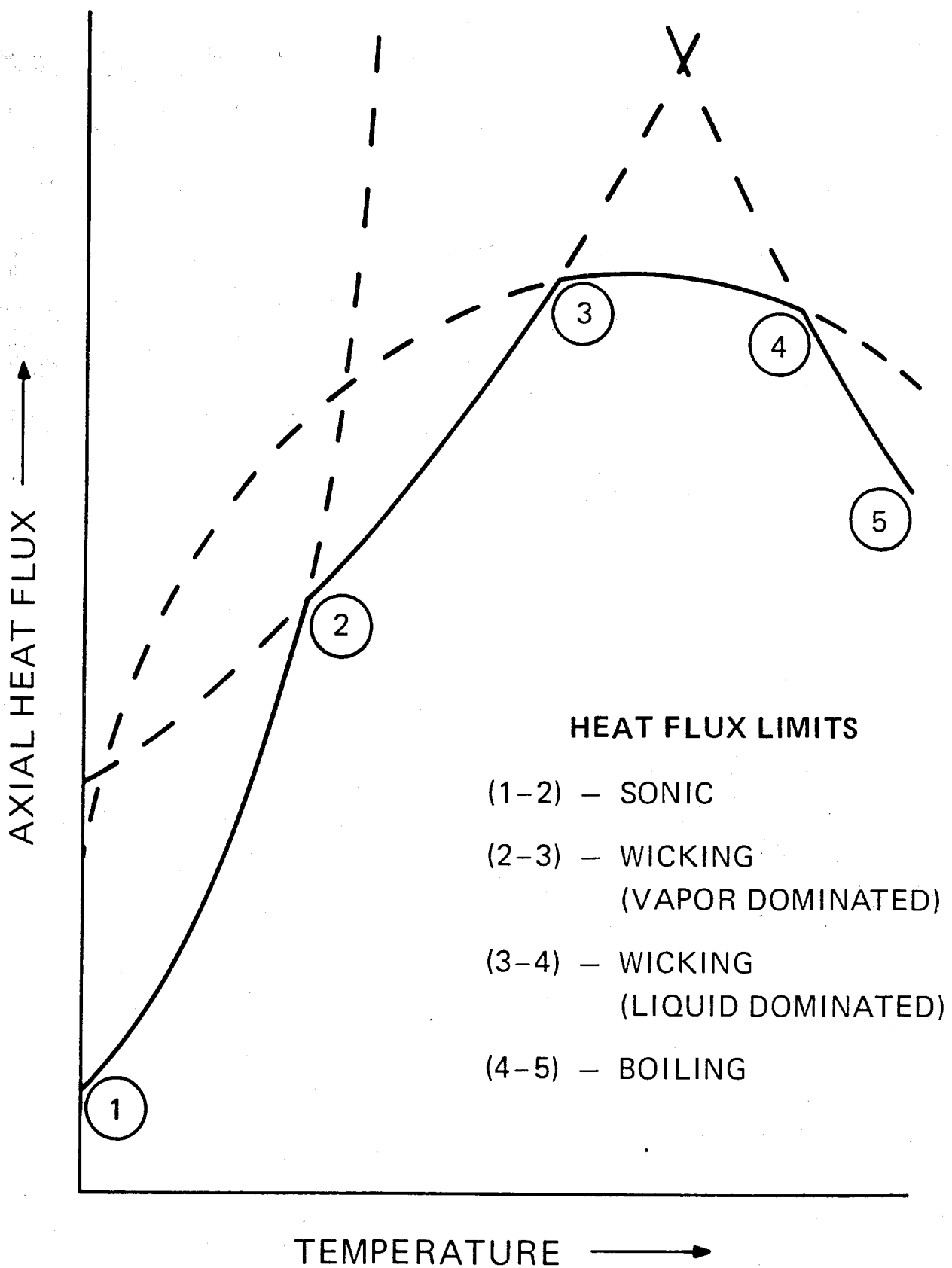
*Typical Performance Parameters for Space  
Reactor Heat Pipe*

<b>Working Fluid</b>	<b>Li</b>
<b>Op. Temp. ° C</b>	<b>1200</b>
<b>Axial Power Density</b>	
<b>Normal</b>	<b>8 kW/cm<sup>2</sup></b>
<b>Contingency</b>	<b>10.5 kW/cm<sup>2</sup></b>
<b>Max. Radial Power</b>	
<b>Evaporator</b>	<b>105 W/cm<sup>2</sup></b>
<b>Condensor</b>	<b>6.5 W/cm<sup>2</sup></b>
<b>Reliability</b>	
<b>7 y normal</b>	<b>98 %</b>
<b>7 y contingency</b>	<b>96 %</b>

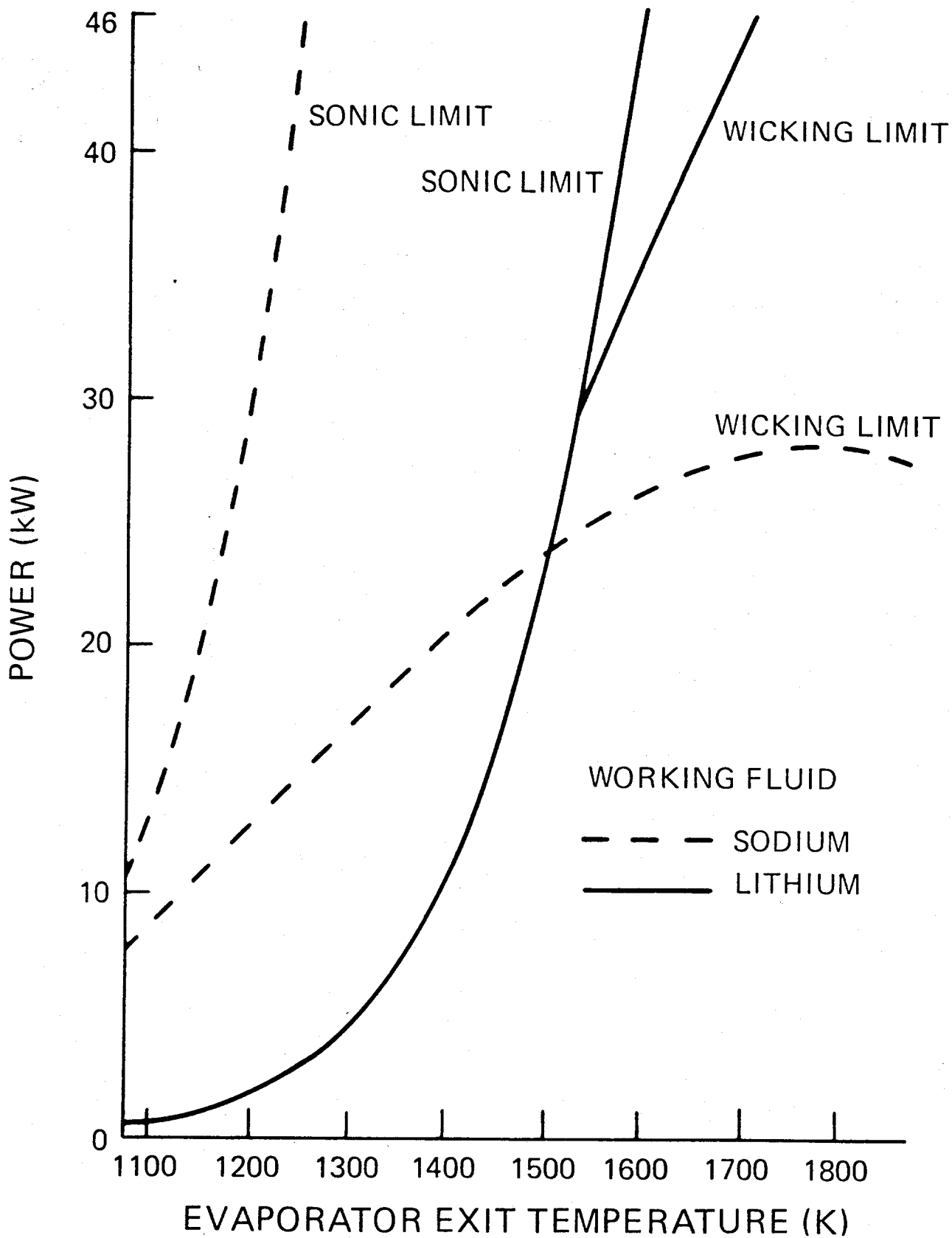


## Transport Limitations

- **Sonic Limits**
  - **Choked Vapor Flow**
  - **Typically occurs when pipe operates near the freezing point where vapor pressures and densities are very low.**
- **Entrainment Limit**
  - **High velocity vapor flow strips and entrains liquid droplets thereby impeding liquid flow to evaporator**
  - **Occurs at high loads and near freeze point**
- **Capillary Pumping**
  - **Hydrodynamic balance between capillary forces and liquid/vapor viscous pressure drops**
  - **Usually determines limiting performance**
- **Boiling Heat Flux**
  - **High local heat fluxes that cause nucleate boiling and interrupts liquid flow in evaporator**



**Fig. 4.11** Phenomena limiting heat pipe performance. *Courtesy of Los Alamos National Laboratory.*



**Fig. 4.12** A comparison of lithium and sodium heat pipe performance. *Courtesy of Los Alamos National Laboratory.*

# HEAT PIPE APPLICATIONS IN SPACE NUCLEAR POWER

## DEMONSTRATED RADIAL FLUX DENSITIES

POTASSIUM 40 TO 50 W/CM<sup>2</sup>

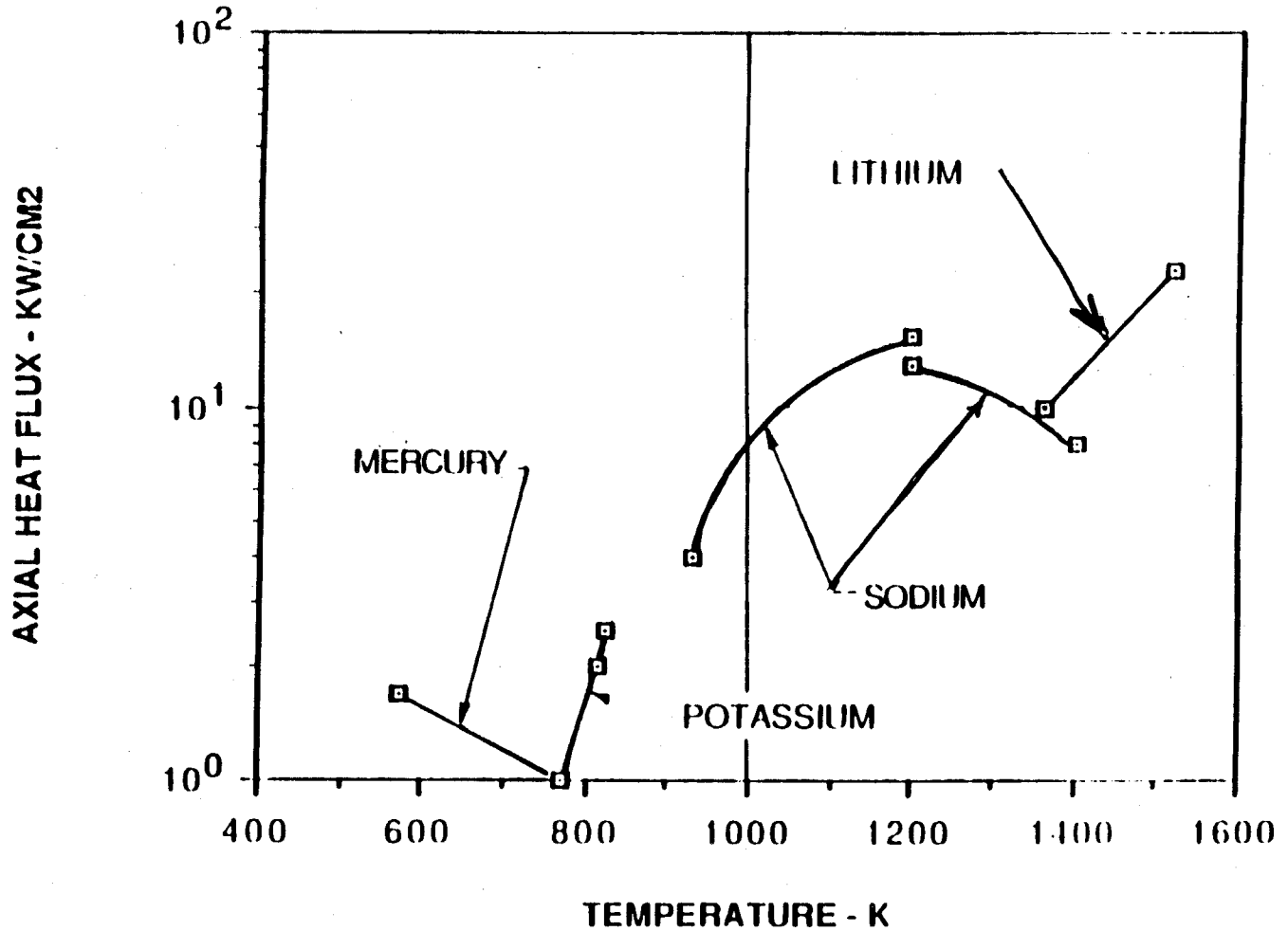
SODIUM TO 1000 W/CM<sup>2</sup>

LITHIUM TO 300 W/CM<sup>2</sup>

MERCURY 150-200 W/CM<sup>2</sup>

# HEAT PIPE APPLICATIONS IN SPACE NUCLEAR POWER

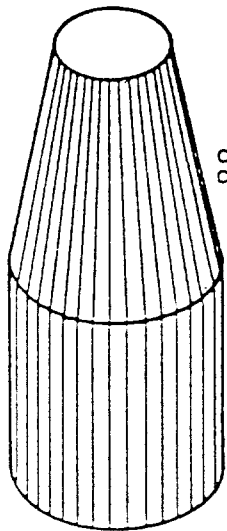
## DEMONSTRATED AXIAL HEAT FLUX



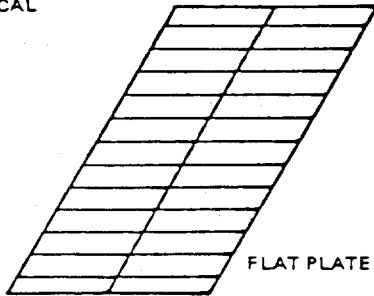
# HEAT PIPE APPLICATIONS IN SPACE NUCLEAR POWER

## DEMONSTRATED OPERATING LIFE FOR HIGH TEMPERATURE HEAT PIPES (LOS ALAMOS)

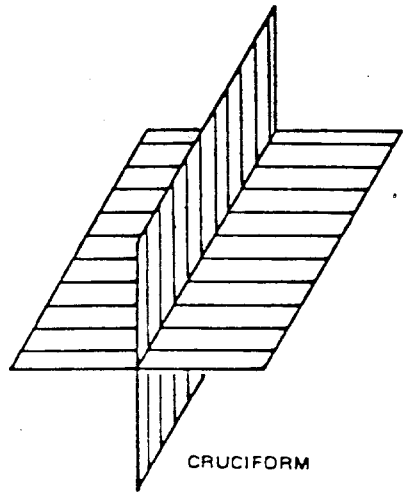
LITHIUM-MOLYBDENUM	25,000 HR @ 1700K
SODIUM-MOLYBDENUM	45,000 HR @ 1400K
SODIUM-300 SERIES SS	23,000 HR @ 920K
POTASSIUM-NB-1ZR (SP-100 TESTS)	10,000 HR @ 1350K
POTASSIUM-300 SERIES SS	5,300 HR @ 920K
POTASSIUM-TITANIUM (REFLUXING CAPSULE)	5,000 HR @ 800K
MERCURY-300 SERIES SS	10,000 HR @ 600K



CYLINDRICAL/  
CONICAL

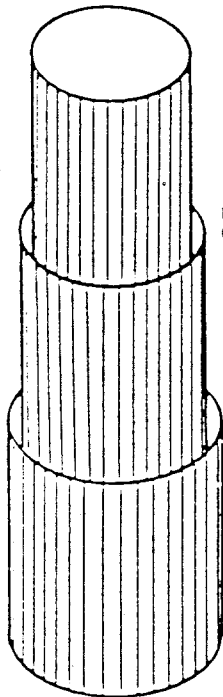


FLAT PLATE

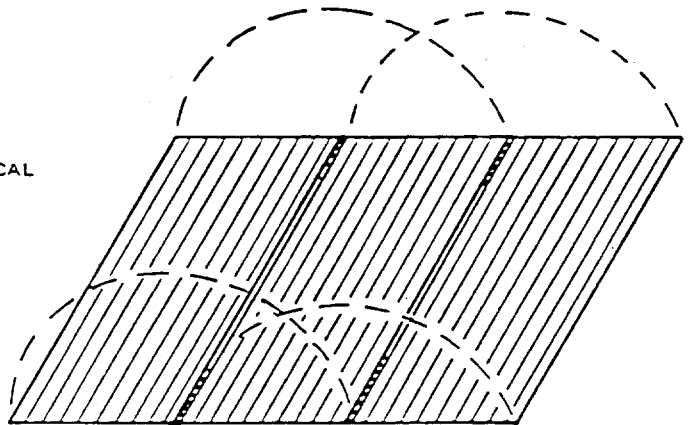


CRUCIFORM

FIXED RADIATORS



NESTED  
CYLINDRICAL

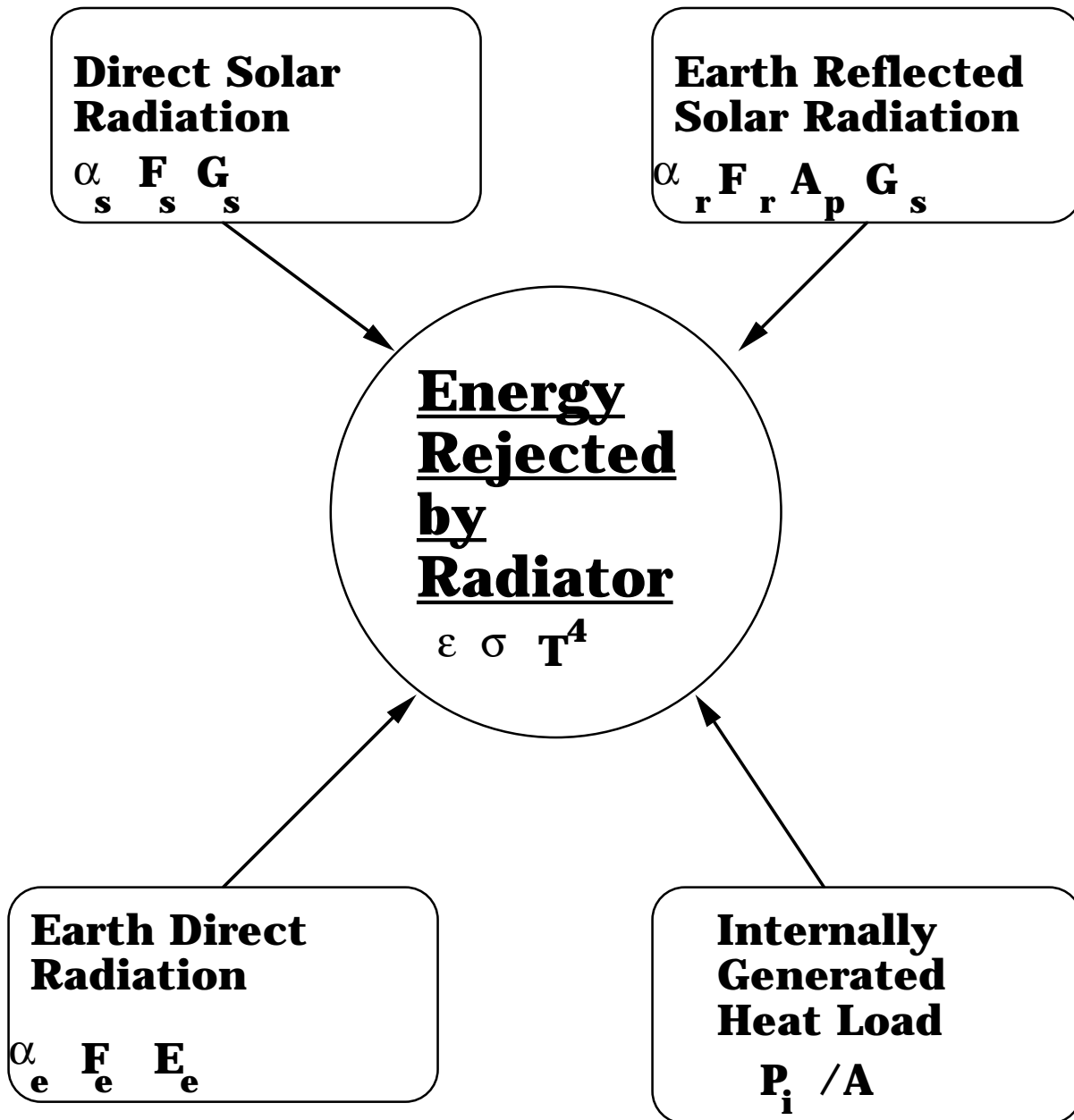


FOLDED FLAT PLATE

DEPLOYABLE RADIATORS

Fig. 6.3 Typical radiator configurations [2].

# Radiator Thermal Design



$\alpha$ =solar absorptivity= 0-1.0 (direct or reflected from the Earth)

$F_s$ =cosine of angle to sun = 0-1.0

$G_s$ =solar constant= 1371 W/m<sup>2</sup> at 1 AU

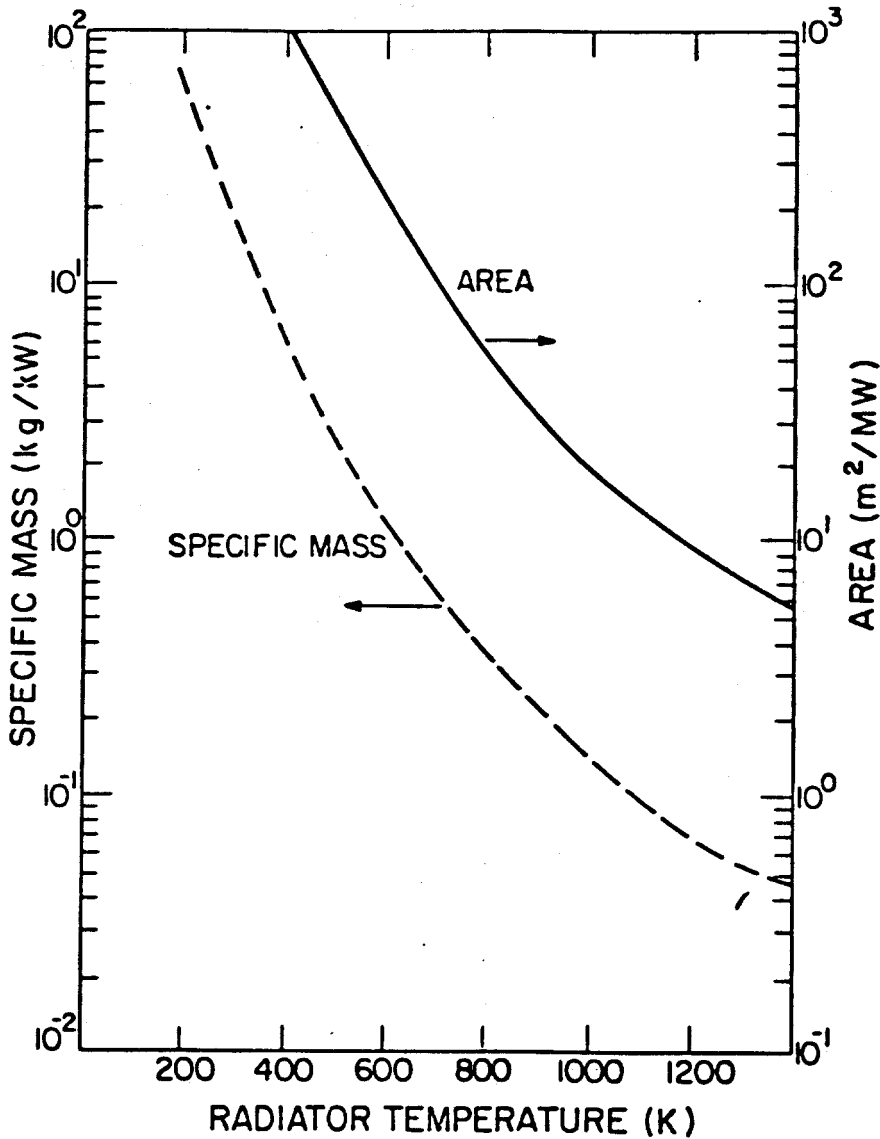
$F_r$ =view factor  $\approx$  0.1 from low Earth orbit, 0.02 from GEO

$A_p$ =Earth's albedo  $\approx$  0.3

$F_e$ =view factor of radiation emitted from the Earth to radiator  $\approx$  0.3

$E_e$ =Earthshine radiation  $\approx$  240 W/m<sup>2</sup>





**Fig. 6.1** Radiator area and mass as a function of temperature.

# RADIATOR WEIGHT DOMINATES LARGE SYSTEMS

