

## 13.10 Migration Mechanisms and Growth of Mobile Bubbles

- *Now we let bubbles move too.*
  - *Distinguish between as fabricated ( some He) and equilibrium ( Xe filled ) bubbles*

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### 13.10.1. Atomic Mechanism of Bubble Mobility Due to Surface Diffusion

*Remember, surface atoms are in constant motion, the slightest imbalance can cause bubbles to move.*

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### 13.10.2 Random Bubble Motion

*There are two diffusivities of major importance*

- *Surface Diffusivity ( $D_s$ )*
- *Bubble Diffusivity ( $D_b$ )*

*In chapter 7;*

$$D_s = \frac{s^2}{4} \quad ( 2 \text{ dimensional} )$$

*total jump frequency of molecules on surface*

$$D_b = \frac{b^2}{6} \quad ( 3 \text{ dimensional} )$$

*jump frequency of bubble*

To relate  $D_s$  to  $D_b$ , note that from the cube model of figure 13.18

$$b = \frac{\text{distance that bubble moves}}{\text{\# of jumps to move bubble}} \frac{x}{x}$$

$$= \frac{x}{\frac{l^3}{x}} = \frac{s}{l^3}$$

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For a spherical bubble;

$$b = \frac{\frac{4}{3} R^3}{a_0^3} s$$

Since # of surface atoms =  $\frac{4 R^2}{a_0^2}$

Frequency of bubble jumps;

$$b = \frac{4 R^2}{a_0^2} s$$

This gives;

$$D_b = \frac{3 a_0^4 D_s}{2 R^4}$$

or;

$$D_b = \left[ \frac{3a_o^4 D_{so}}{2} \exp - \frac{E_s}{kT} \right] \cdot \frac{1}{R^4}$$

***Small bubbles move faster than large ones***

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**13.10.3 Directed Bubble Migration in a Temperature Gradient**

***Introduction of bubble disturbs temperature profile ( see figure 13.19)***

One finds that ;

$$\frac{dT}{dx}_b > \frac{dT}{dx}_{normal}$$

or;

$$\frac{dT}{dx}_b = \frac{3}{2} \frac{dT}{dx}$$

Note that the flux of atoms along surfaces (chapter 7) is;

$$J_s = - \frac{D_s Q_s^* C_s}{kT^2} \cdot \frac{dT}{dx}_b$$

and;

$$v_b = - \frac{3D_s Q_s^* a_o}{kT^2 R} \cdot \frac{dT}{dx}$$

Note  $Q_s^*$  (heat of transport) must be positive because bubbles move up a temperature

**gradient**

**Olander calculates for**

$$\mathbf{R = 100 \text{ \AA} \quad a_0 = 3 \text{ \AA} \quad T = 1000^\circ\text{K}}$$

$$Q_s^* = 415 \frac{\text{kJ}}{\text{mole}} \frac{dT}{dx} = 4000 \frac{^\circ\text{K}}{\text{cm}}$$

$$D_s = 5 \times 10^{-7} \frac{\text{cm}^2}{\text{sec}}$$

**gives;**

$$v_b = 3 \times 10^{-6} \frac{\text{cm}}{\text{sec}}, \quad 0.2592 \frac{\text{cm}}{\text{day}}$$
$$1.814 \frac{\text{cm}}{\text{week}}$$

***But T changes with time, so we cannot extrapolate too long***

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### **13.10.4 General Treatment of Bubble Mobility**

**Fred Nicols (now at ANL) has been a major contributor in this area**

$$v_b = \text{mobility} \times \text{force} = M_b F_b = \frac{D_b F_b}{kT}$$

**Nicols relates macroscopic and microscopic forces to find;**

$$F_b = \frac{2 R^3}{a_0^3} \frac{Q_s^*}{T} \frac{dT}{dx}$$

### 13.10.5 Bubble Migration by Volume Diffusion

**Consider the effect of vacancy motion outside the bubble**

**Need to get new expressions for bubble jump frequency and jump distance.**

**{ See Figure 13.20 }**

**Assuming that a bubble is a perfectly absorbing sphere;**

**Jump distance**

$$b = \frac{4 R^2 D_{vol}}{a_o^4}$$

$$b = \frac{3a_o^3}{4 R^3} \cdot \sqrt{\frac{2}{v}}$$

**Problem of determining this distance has been treated by Olander**

$$\sqrt{\frac{2}{v}} = 2 R a_o$$

**Remember that**

$$D_b = \frac{b^2}{6}$$

**Which produces ( for Brownian motion);**

$$D_b = \frac{3a_o^3}{4} \frac{1}{R^3} D_{vol}$$

**For surface diffusion  $D_b$   $\frac{1}{R^4}$  Have to get for moving species**

**Next, consider the effect of a temperature gradient;**

$$v_b = \frac{D_b F_b}{kT}$$

$$\text{where } F_v = - \frac{Q_v^*}{T} \cdot \frac{dT}{dx}_b$$

**and  $Q_v^*$  = heat of vacancy transport energy of self diffusion**

***Nicols finds;***

$$v_b = \frac{D_{vol} Q_v^*}{kT^2} \cdot \frac{dT}{dx}$$

**Problem 13.2**

## Problem 13.2

a.) What is the root mean squared distance traveled in 40 days by a 20 Å diameter bubble undergoing Brownian motion in  $\text{UO}_2$  at 1400 °C

b.) Recalculate a.) in a temperature gradient of 2000 °C/cm

Assume that the bubble diffusivity is governed by surface diffusion and  $Q_s^* = 415$  kJ/mole

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a.) From Ch. 7

$$r^2 = 6D_b t = \frac{9a_o^4 D_s t}{R^4}$$

eq. 13.214

use  $a_o = 3 \text{ \AA}$

$$t = 40 \cdot 24 \cdot 3600 = 3.46 \times 10^6 \text{ s}$$

$$R = 10 \text{ \AA}$$

$$T = 1400^\circ\text{C} = 1673 \text{ K}$$

eq. 13.216

$$D_s = 4 \times 10^5 \cdot \exp(-108/RT) \text{ cm}^2/\text{s}$$

$$= 2.77 \times 10^{-9} \text{ cm}^2/\text{s}$$

$$\sqrt{r^2} = \frac{9 \cdot 3^4 \cdot 2.77 \times 10^{-9} \cdot 3.46 \times 10^6}{10^4}^{\frac{1}{2}}$$

$$= 0.015 \text{ cm}$$

## b.) Thermal Gradient Migration

eq 13.219

$$r = \frac{3D_s Q_s^* a_o}{RkT^2} \cdot \frac{dT}{dx} t$$

$$r = \frac{3 \cdot 2.77 \times 10^{-9} \cdot 100 \times 10^3 \cdot 4.18 \cdot 3 \cdot 2000 \cdot 3.46 \cdot 10^6}{10 \cdot 1.38 \times 10^{-23} \frac{\text{J}}{\text{K}} [1673]^2 \cdot 6.02 \times 10^{23}}$$

$$= 0.310 \text{ cm}$$

In other words, the bubble moves almost 21 times farther in a temperature gradient



### 13.10.6 Bubble Migration in a Stress Gradient

Trick is to calculate the force on a bubble as it moves from  $x$  to  $x + dx$  and the stress changes from  $\sigma$  to  $\sigma + d\sigma$ .

$$F_b = -\frac{dG_b}{dx} \quad (\text{at constant temp.})$$

Gibbs free energy of bubble

Three contributions to  $G_b$ ;

- 1.) Change in free energy of contained gas,  $dG_g$
- 2.) Change in free energy of system due to change in surface area,  $dG_s$
- 3.) Change in strain energy of solid,  $dE_{\text{solid}}$

For an Ideal Gas;

$$dG_b = -p dV = -p(4\pi R^2 dR)$$

For surface energy;

$$dG_s = 8\pi R dR$$

or, 
$$dG_g + dG_s = -4 R^2 p - \frac{2}{R} dR$$

since  $p - \frac{2}{R} =$

Need to get this in terms of x  
Use;

$$+ \frac{2}{R} \cdot \frac{4 R^2}{3} = mkT$$

differentiating;

$$\frac{dR}{d} = - \frac{R^2}{3 R + 4}$$

but,

$$dR = \frac{dR}{d} \cdot \frac{d}{dx} dx$$

So;

$$dR = - \frac{R^2}{3 R + 4} \cdot \frac{d}{dx} dx$$

This gives;

$$\frac{dG_g}{dx} + \frac{dG_s}{dx} = \frac{4 R^4}{3 R + 4} \frac{d}{dx}$$

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For elastic energy, start with

$$E_{el} = \frac{2}{2K} \quad \text{Bulk Modulus}$$

and end up with;

$$\frac{dE_{solid}}{dx} = - \frac{2 R^3}{3K} \cdot \frac{3 R + 8}{3 R + 4} \cdot \frac{d}{dx}$$

Put it all together;

$$F_b = - \frac{4 R^2}{3 R + 4} \cdot 1 - \frac{3 R + 8}{6RK} \cdot \frac{d}{dx}$$

For small bubbles and  
bubbles

low  
stresses;

$$3 R \ll 4$$

For large

and high

$$F_b = - \frac{R^4}{3} \cdot \frac{d}{dx}$$

$$F_b = - \frac{4 R^3}{3} \cdot \frac{d}{dx}$$

**Bubbles always move down a  
stress gradient !**

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$$\frac{(F_b)_{stress}}{(F_b)_{temp}} = \frac{(R^2 a_o^3)}{2 kT \frac{Q^*}{kT}} \cdot \frac{\frac{1}{T} \frac{d}{dx}}{\frac{1}{T} \frac{dT}{dx}} \quad \mathbf{0.01}$$

### 13.10.7 Bubble Growth by Coalescence

**Two main contributors;**

- **Greenwood and Speight (1963)**
- **Gruber (1967)**

**Both assumed ;** • **perfect gas**

- **mechanical equilibrium**
- **Surface diffusion**
- **Random or gradient migration**
- **No resolutioning**
- **No pinning**

#### Greenwood and Speight Model

- **Did not consider directed motion;**

**1.) Post Irradiation Annealing**

- **Perfect Gas**
- **No Size Distribution**

$$R = 1.48 \frac{a_o^4 D_s M k T}{t^{\frac{1}{5}}}$$

**number of gas atoms/cc**

**2.) In -Pile**

$$Y_{Xe} Ft = mN$$

$$\frac{dN}{dt} = \frac{Y_{Xe} \dot{F}}{m} - 16 RD_b N^2$$

**assumes that all bubbles are born at R**

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after several steps;

$$R = 1.28 \frac{a_o^4 D_s Y_{Xe} \dot{F} kT}{t^{\frac{1}{5}}} t^{\frac{2}{5}}$$

and swelling

$$\frac{V}{V} = 1.48 \left( a_o^4 D_s \right)^{\frac{1}{5}} Y_{Xe} \dot{F} \frac{kT}{2} t^{\frac{6}{5}} t^{\frac{7}{5}}$$

*This over predicts the swelling because it does not account for gas atoms escaping*

### Gruber's Method

He considered the

a.) production, and

b.) destruction of m sized bubbles

*After a great deal of more exact formulations;*

$$R = 1.32 \frac{a_o^4 D_s m kT}{t^{\frac{1}{5}}} t^{\frac{1}{5}}$$

remember that S&G used 1.48

### Figure 13.22

Note how much more effective coalescence is than single atom absorption

**However both predictions are too optimistic because of neglecting of pinning to dislocations and G.B.'s**

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**Improvements**

$$\begin{aligned} \frac{dC_m}{dt} = & k_{1,m-1} C C_{m-1} - k_{1,m} C C_m - b' C_m \\ & + \frac{1}{2} \left( 1 + \frac{j}{m} \right) k_{m-j,j} C_{m-j} C_j \\ & - \left( 1 + \frac{j}{m} \right) k_{m,j} C_m C_j \end{aligned}$$

**But still have not included**

- **spatial variations of defect concentration**
- **No pinning**

**13.11 Pinning of Bubbles by Dislocations and Grain Boundaries**

- **Vacancy Clusters**
- **Interstitial Clusters**
- **Precipitates of FP**
- **Dislocation Lines**
- **Grain Boundaries**

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**Model see figure 13.23 for dislocations**

$$F_b = 2t_d \cos F$$

**line tension**

**If dislocation and temperature gradient is perpendicular, then,**

$$R_d = \frac{a_o^3 b^2 G T}{Q_s^* \frac{dT}{dx}} \quad \frac{1}{3}$$

**critical pulloff radius**

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**Grain Boundaries**

**See Figure 13.24**

**let  $\gamma_{gb}$  = grain boundary tension**

$$F_b = 2 R \gamma_{gb} \sin \theta \cos \theta$$

**when  $\gamma_{gb} = 300$  dynes/cm  
critical radius = 4000 Å**

**Study Figure 13.25 for critical bubble radii**

- **Note that surface diffusion is more important in UO<sub>2</sub>**
  - **Because of better thermal conductivity, there is a lower dT/dx**
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### **13.12 Bubl Code**

**(Transport) • Grass Code - C.Y. Li -  
coalescence**

**(Monte Carlo) • Bubl Code - Nicols - includes  
pinning**

***In Bubl code***

- 1.) Bulk coalescence neglected***
- 2.) Resolution neglected***
- 3.) Nucleation ignored***

**Cell approach - Fig. 13.26 - size of grains**

- all gas starts out as small uniform sized bubbles**
- Coalescence can occur on dislocation by adjacent bubbles growing or by flux of incident bubbles**
- Bubbles move until they hit GB**
- Released at cracks**

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**Swelling due to**

- 1.) Bubbles at dislocations**
- 2.) Bubbles in transit from disloc. to GB**
- 3.) Bubbles trapped at GB**

## **4.) Bubbles in transit from GB to cracks**